

Introducing Some Correlations to Calculate Entropy Generation in Extended Surfaces with Uniform Cross Sectional Area

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ABSTRACT

The optimum length of extended surfaces with uniform cross sectional area has been analyzed numerically, based on the concept of entropy generation minimization. The extended surface studied is a pin fin. The rate of entropy generation is investigated for different boundary conditions. First, some correlations are introduced to calculate this rate, and then a model is offered to find optimum length of the fin for adiabatic and convection heat transfer boundary conditions. The accuracy of the model presented is compared with experimental data. Although Bejan introduced a correlation to calculate optimal Reynolds number and consequently the optimum length of a pin fin, but the results showed the new method has high accuracy compared with the Bejan method. Also, it is found that there is a strong relation between optimum length (based on the entropy generation minimization concept) in one side, and temperature distribution in the other side.

Keywords: Entropy generation minimization, Optimum length, Pin fin, Temperature distribution

1. INTRODUCTION

The entropy generation in the process is due to irreversibilities occurring inside the system. This internal entropy generation can be caused by the friction, unrestrained expansions, and the internal transfer of energy over a finite temperature difference. In addition to this internal entropy generation, external irreversibilities are possible by heat transfer over finite temperature differences as the δQ is transferred from a reservoir or by the mechanical transfer of work. Equation of (1) is valid with the equal sign for a reversible process and the greater than sign for an irreversible process. Since the entropy generation is always positive and the smallest in a reversible process, namely zero, it may deduce some limits for the heat transfer and work terms.

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Nomenclature			
A_c	cross sectional area	Re	Reynolds number
C_D	drag coefficient	$\dot{S}_{gen}$	entropy generation
D	diameter	T	temperature
F_D	drag force	U_∞	velocity
H	enthalpy	W	work
h	convective coefficient	Greek letter symbols	
k	thermal conductivity	ρ	density
L	length	λ	air thermal conductivity
$\dot{m}$	mass flow rate	μ	dynamic viscosity
Nu	Nusselt number	ν	kinematic viscosity
N_s	entropy generation number	Subscript	
P	pressure	b	base
Pr	Prandtl number	∞	ambient
p	perimeter		
q	heat transfer rate		

$$\left\{ \begin{array}{l} dS = \frac{\partial Q}{T} + \partial S_{gen} \\ \partial S_{gen} \geq 0 \end{array} \right. \quad (1)$$

Considering a reversible process, for which the entropy generation is zero, the heat transfer and work terms therefore are:

$$\partial Q = T.dS \quad \text{and} \quad \partial W = P.dV \quad (2)$$

For an irreversible process with a nonzero entropy generation, the heat transfer becomes,

$$\partial Q_{irr} = T.dS - T.\partial S_{gen} \quad (3)$$

And thus is smaller than that for the reversible case for the same change of state, dS . Furthermore, the work is no longer equal to PdV but is smaller.

$$\partial W_{irr} = P.dV - T.\partial S_{gen} \quad (4)$$

Showing that the work is reduced by an amount proportional to the entropy generation. For this reason, the term $T.\partial S_{gen}$ is often called *lost work*. Although it is not a real work or energy quantity lost but rather a lost opportunity to extract work. So, minimizing entropy generation is very important in many industries. One of the this applications is in the heat exchanger industry. The compact heat exchangers are widely used in automobile, chemical, petrochemical, air-conditioning systems, oil, and food industry, and therefore using optimization by entropy minimization play a key role in saving energy, and decreasing environmental pollution. Bejan [1] was one of the first researchers who considered the entropy generation minimization in convective heat transfer. Asadi and Khoshkhoo [2-5] carried out some researches about transferring heat by radiation in the Plate-Fin heat exchanger. Based on their research the amount of the heat transferring using radiation is just 2% compared with convection in the Plate-Fin heat exchanger and Finned-Tube heat exchangers. Hence, we can ignore radiation in the Plate-Fin heat exchanger with a good approximation in order to minimize entropy generation.

Many researchers investigated about optimization using minimizing entropy generation [6-38]. However, the topic of entropy generation in extended surfaces was remained unexplored. Entropy generation minimization was first introduced by McClintock [39], who developed equations for optimum design of fluid passages for a heat exchanger. Then, Bejan [1] examined the coupling losses due to heat transfer across a finite temperature difference and frictional pressure drop. He used the number of entropy generation units, N_s , as a basic parameters in analyzing the heat exchanger performance. Establishing the theoretical framework for the minimization of entropy generation was done by Poulikakos and Bejan [40]. However in recent years, many heat exchanger tools were introduced based on the concept of entropy generation minimization. For example, Radermacher [42] studied on a numerical approach for modeling of air-to-refrigerant Fin-and-Tube heat exchanger with Tube-to-Tube heat transfer. Liu et.al, [41] presented a general steady state mathematical model for fin-and-tube heat exchanger. Jiang and Radermacher [42] offered a general-purpose simulation and design tool for air-to-refrigerant heat exchangers. Entropy generation minimization of a double-pipe pin fin heat exchanger was analyzed by Sahiti and Krasniq [43]. They derived their results on the basis of the behavior of entropy generation number as a definition of Reynolds number. They concluded that not all definition forms for the entropy generation number leads to the right conclusions. Thermal hydraulic design of fan-supplied tube-fin condenser for refrigeration was investigated experimentally by Hermes and Waldyr [44]. Ibrahim and Moawad [45] carried out an experimental investigation to clarify heat transfer characteristics and entropy generation for individual elliptic tubes with Longitudinal fins. The investigated geometrical parameters included the placement of the fins at the front of the tube, at the rear of the tube and at the front and rear of the tube. The results indicated that the fin position on the elliptic tubes has as effect on the results of heat transfer coefficient, friction factor, and irreversibility ratio. Zhang and Yang [46] introduced a distributed parameter model in optimization the plate-fin heat exchanger based on the minimum entropy generation. Huee and Lee [47] conducted an analytical study on optimal design of refrigerant circuitry of fin-and-tube condenser based on the entropy generation minimization. They validated their model by comparing their numerical results with experimental data for an R410A multi-pass condenser. The resulting refrigerant circuit design enhanced heat transfer performance and lowered entropy generation in comparison to simple refrigerant circuitries. The application of the entropy generation minimization method to the pseudo-optimization of the configuration of the heat exchange surfaces in a solar Rooftile was studied by Giorgio et.al, [48]. He found that the geometry with pin-fins has the best performance, and the optimal pin array shape parameters can be determined by a critical analysis of the integrated and local entropy maps and of the temperature contours. Pussoli and Barbasa [49] presented an investigation in optimization of peripheral finned-tube evaporators using entropy generation minimization. They experimentally validated semi-empirical models for the air-side heat transfer and pressure drop with entropy generation minimization theory to determine the optimal characteristics of peripheral finned-tube heat exchanger. Minimizing the entropy generation rate of the plate-finned heat sinks using computational fluid dynamics and combined optimization was carried out by Zhou and Yang [50]. The results showed that the overall rate of entropy generation decreases as the result of introducing the additional constrained variables into the optimization process. Gediz et.al, [51] focused on the effect of aspect ratio on entropy generation in a rectangular cavity with differentially heated walls. Aggrey and Tunde [52] presented the results of a numerical analysis of entropy generation in a parabolic trough receiver at different concentration ratios, inlet temperatures and flow rates. The results showed that there is an optimal flow rate at which the entropy generated is minimum, for every combination of concentration ratio and inlet temperature. Wenhua, Xuan and Jian [53] analyzed entropy generation of fan-supplied gas cooler within the framework of two-stage CO_2 transcritical refrigeration cycle. They suggested that the analysis with isolated gas cooler can lead to overestimated or unrealistic

predictions on the heat transfer performance compared to the analysis within the framework of entire cycle.

In this paper a pin fin is analyzed for the rate of entropy generation. After introducing some correlations to calculate the entropy generation rate, optimization process has been done. Finally, the optimum value of fin length is compared with experimental studies.

2. MATHEMATICAL DESCRIPTION

There is an important relationship between lost available work and entropy generation.

$$\begin{cases} \dot{W}_{\text{lost}} = T \cdot \dot{S}_{\text{gen}} \\ \dot{S}_{\text{gen}} = \frac{\partial S}{\partial t} - \frac{Q}{T} - \sum_{\text{in}} \dot{m} S + \sum_{\text{out}} \dot{m} S \end{cases} \quad (5)$$

This equation represents the Gouy-Stodola theorem. This theorem states that the lost available work is directly proportional to the entropy production. The terms of entropy production is arising heat transfer and fluid friction. For the entropy production due to heat transfer:

$$\begin{aligned} \dot{S}_{\text{gen}} dx dy = & \frac{q_x + \frac{\partial q_x}{\partial x} dx}{T + \frac{\partial T}{\partial x} dx} dy + \frac{q_y + \frac{\partial q_y}{\partial y} dy}{T + \frac{\partial T}{\partial y} dy} dx - \frac{q_x}{T} dy - \frac{q_y}{T} dx + \left(s + \frac{\partial s}{\partial x} dx \right) \left(v_x + \frac{\partial v_x}{\partial x} dx \right) \left(\rho + \frac{\partial \rho}{\partial x} dx \right) dy \\ & + \left(s + \frac{\partial s}{\partial y} dy \right) \left(v_y + \frac{\partial v_y}{\partial y} dy \right) \left(\rho + \frac{\partial \rho}{\partial y} dy \right) dx - s v_x \rho dy - s v_y \rho dx + \frac{\partial(\rho s)}{\partial t} dx dy \end{aligned} \quad (6)$$

For the two-dimensional Cartesian system,

$$\dot{S}_{\text{gen}} = \frac{k}{T^2} \left[\left(\frac{\partial T}{\partial x} \right)^2 + \left(\frac{\partial T}{\partial y} \right)^2 \right] + \frac{\mu}{T} \left\{ 2 \left(\frac{\partial v_x}{\partial x} \right)^2 + \left(\frac{\partial v_y}{\partial y} \right)^2 \right\} + \left(\frac{\partial v_x}{\partial x} + \frac{\partial v_y}{\partial y} \right)^2 \quad (7)$$

And for friction factor,

$$\dot{S}_{\text{gen}} = \dot{m} \left(\int_{\rho_{\text{out}}}^{\rho_{\text{in}}} \frac{v}{T} dP \right)_{h=\text{constant}} \quad (8)$$

Recently, the Bejan number was named by Paoletti. Accordingly Be=1 is the limit at which the heat transfer irreversibility dominates, Be=0 is the opposite limit at which the irreversibility is dominated by fluid friction effects, and Be=0.5 is the case in which the heat transfer and fluid friction entropy generation rates are equal.

For the external flow, there are three thermodynamic statements,

$$\dot{m}_{\text{in}} = \dot{m}_{\text{out}} = \dot{m} \quad (9)$$

$$\dot{m} h_{\text{in}} + \iint q'' dA - \dot{m} h_{\text{out}} = 0 \quad (10)$$

$$\dot{S}_{\text{gen}} = \dot{m} s_{\text{out}} - \dot{m} s_{\text{in}} - \iint \frac{q'' dA}{T_w} \quad (11)$$

Where T_w is the temperature of wall. The canonical form $dH = T ds + \left(\frac{1}{\rho} \right) dP$ may be written:

$$H_{\text{out}} - H_{\text{in}} = T_{\text{ave}} (s_{\text{out}} - s_{\text{in}}) + \frac{1}{\rho} (P_{\text{out}} - P_{\text{in}}) \quad (12)$$

Combination Equations (11) and (12) the entropy generation rate will be:

$$(\dot{S}_{gen})_{external} = \iint_A q'' \left(\frac{1}{T_{\infty}} - \frac{1}{T_w} \right) dA + \frac{F_D U_{\infty}}{T_{\infty}} \quad (13)$$

Also, a fin generates entropy internally, because the fin is nonisothermal,

$$(\dot{S}_{gen})_{internal} = \iint_A \left(\frac{q''}{T_w} \right) dA - \frac{q_B}{T_b} \quad (14)$$

In this expression, q_B and T_b represent the base heat transfer and absolute temperature. Adding Equations of (13) and (14) side by side obtaining the entropy generation rate for a single fin is possible.

$$\dot{S}_{gen} = \frac{q_B \theta_B}{T_{\infty}^2} + \frac{F_D U_{\infty}}{T_{\infty}} \quad (15)$$

Where θ_B is the base-stream temperature difference ($T_b - T_{\infty}$). Also, Drag coefficient for a pin fin is:

$$\begin{cases} C_D = \frac{F_D}{\frac{1}{2} \rho U_{\infty} D L} \\ C_D \cong 5.484 Re^{-0.246} \end{cases} \quad (16)$$

Needing to the rate of heat transfer, q , in order to calculate the entropy generation is necessary. The rate of heat transfer can be calculated for different conditions. Applying the conservation of energy requirement results in:

$$\frac{d^2 T}{dx^2} + \left(\frac{1}{A_c} \frac{dA_c}{dx} \right) - \left(\frac{1}{A_c} \frac{h}{k} \frac{dA_s}{dx} \right) (T - T_{\infty}) = 0 \quad (17)$$

For the uniform profile, A_c , is constant and $A_s = Px$ where A_s is the surface area measured from the base to x , and P is the fin perimeter. So,

$$\frac{d^2 T}{dx^2} - \frac{hP}{kA_c} (T - T_{\infty}) = 0 \quad (18)$$

Bejan et.al, (1995) solved this equation, and suggested some correlations to calculate the rate of entropy production based on the adiabatic conditions on the tip fin. Here, our focus is on the remained conditions, very long fin, and Convection heat transfer. So, for Convection heat transfer, the rate of heat transfer is:

$$q = \sqrt{hPkA_c} (T_b - T_{\infty}) \frac{\sinh(mL) + (h/mk) \cosh(mL)}{\cosh(mL) + (h/mk) \sinh(mL)} \quad (19)$$

Where,

$$m = \sqrt{\frac{hP}{kA_c}} \quad \text{and} \quad M = \sqrt{hPkA_c} \theta_b \quad (20)$$

And using Equation of (15), the rate of entropy generation will be:

$$\dot{S}_{gen} = \left\{ (hPkA_c)^{0.5} \cdot \left(\frac{T_b}{T_{\infty}} - 1 \right)^2 \cdot \left(\frac{\sinh(mL) + (h/mk) \cosh(mL)}{\cosh(mL) + (h/mk) \sinh(mL)} \right) \right\} + \left\{ \frac{2.742 (\rho D)^{0.754} \cdot U_{\infty}^{2.754} \cdot \mu^{0.246} \cdot L}{T_{\infty}} \right\} \quad (21)$$

Similarity for adiabatic boundary condition, the rate of entropy generation is:

$$\dot{S}_{gen} = \left\{ (hPkA_c)^{0.5} \cdot \left(\frac{T_b}{T_\infty} - 1 \right)^2 \cdot \tanh(mL) \right\} + \left\{ \frac{2.742(\rho D)^{0.754} \cdot U_\infty^{2.754} \cdot \mu^{0.246} \cdot L}{T_\infty} \right\} \quad (22)$$

Now, calculating the optimum flow length, based on the minimizing entropy generation, is possible.

$$L_{opt,1} = \text{Log} \left[\frac{a_1 \pm \sqrt{a_1^2 + (h/mk)^2 - 1}}{(h/mk) + 1} \right] \cdot m^{-1} \quad (23)$$

$$a_1 = \frac{2\sqrt{M}(T_b - T_\infty)^2 \left[(h/mk)^2 - 1 \right] m}{C_D \cdot U_\infty^3 \cdot D \cdot \rho \cdot T_\infty} \quad (24)$$

These equations dictate the optimum length of flow for the convection heat transfer boundary condition. Also, the optimum length when there is adiabatic boundary condition in system is:

$$L_{opt,2} = m^{-1} \cdot \sinh^{-2}(a_2 - 1) \quad (25)$$

$$a_2 = - \frac{2.742(\rho D)^{0.754} \cdot U_\infty^{2.754} \cdot \mu^{0.246} \cdot T_\infty^2}{m \sqrt{hPkA_c} \theta_b^2} \quad (26)$$

3. VALIDATION

In order to validate results obtained, a comparison of numerically results with experimentally results has been performed. The comparison has been made for a rod 5mm in diameter has one end maintained at 100°C. The surface of rod is exposed to ambient air at 25°C. The convection heat transfer coefficient and thermal conductivity of the fin are 100 and 398 W/m².K respectively. The emissivity and absorptivity of copper are assumed that be 0.83 and 0.13 respectively. The experimental results have been derived from Bejan research on the optimum dimensions of extended surfaces with uniform cross sectional area. He suggested that the number of entropy generation for a rod with adiabatic boundary condition is:

$$N_s = \frac{\left(\frac{k}{\lambda} \right)^{0.5}}{\frac{\pi}{2} Nu^{0.5} Re_D \tanh \left[2Nu^{0.5} \left(\frac{\lambda}{k} \right)^{0.5} \frac{Re_L}{Re_D} \right]} + \frac{1}{2} BC_D Re_L Re_D \quad (27)$$

$$Re_{L,opt} = \frac{Re_D}{2Nu^{0.5}} \left(\frac{k}{\lambda} \right)^{0.5} \sinh^{-1} \left(\left(\frac{8}{\pi C_D B Re_D^3} \right)^{0.5} \right) \quad (28)$$

Also, Masoud Asadi and N.D.Mehrabani [4] presented an equation to determine the optimum diameter versus Reynolds number,

$$Re_{D,opt} = \left\{ 2.38 \frac{8}{\pi C_D B} \right\}^{0.333} \quad (29)$$

In Equation of (27) through (29) Re_D , Re_L and B are respectively:

$$Re_D = \frac{U_\infty D}{\nu} \quad (30)$$

$$Re_L = \frac{U_\infty L}{\nu} \quad (31)$$

$$B = \frac{\rho \nu^3 k T_\infty}{q_B^2} \quad (32)$$

Table.1. Input information

$U_\infty (m/s)$	$\nu (m^2/s)$	$\lambda (W/m^2.K)$	$k (W/m^2.K)$	Pr	$\rho (kg/m^3)$	$L (m)$
20	15.89×10^{-6}	26.3×10^{-3}	398	0.707	1.1614	0.200

Table.2. Thermal quantity results

Re_D	C_D	B	Nu	m	M	$q (W)$
6293.2	0.637	8.14×10^{-12}	30.12	14.17	8.3	8.24

4. DISCUSSION

The validation of numerical method showed that the optimum length of the fin based on the Bejan research is 63 mm, while for the presented method is 223mm. To discuss about the reason of this difference, it is necessary that we notice to the temperature distribution along the fin. Figure of (1) demonstrates the temperature profile for the adiabatic condition.

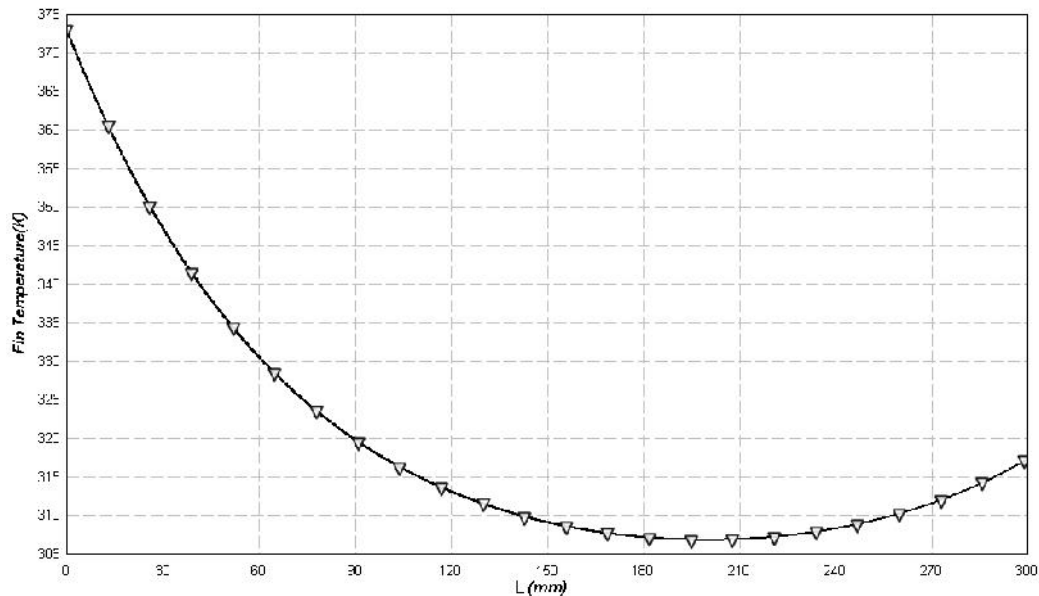


Fig .1. Fin temperature distribution

Moving along the fin the temperature decreases, but there is an inverse trend from $x=225$ onwards. In fact, although temperature decreases with growing the length of the fin, when the fin length reaches to 225 mm there is a moderate increase trend in the temperature profile of the fin. Also, it is useful to see the function of entropy generation for the case study presented.

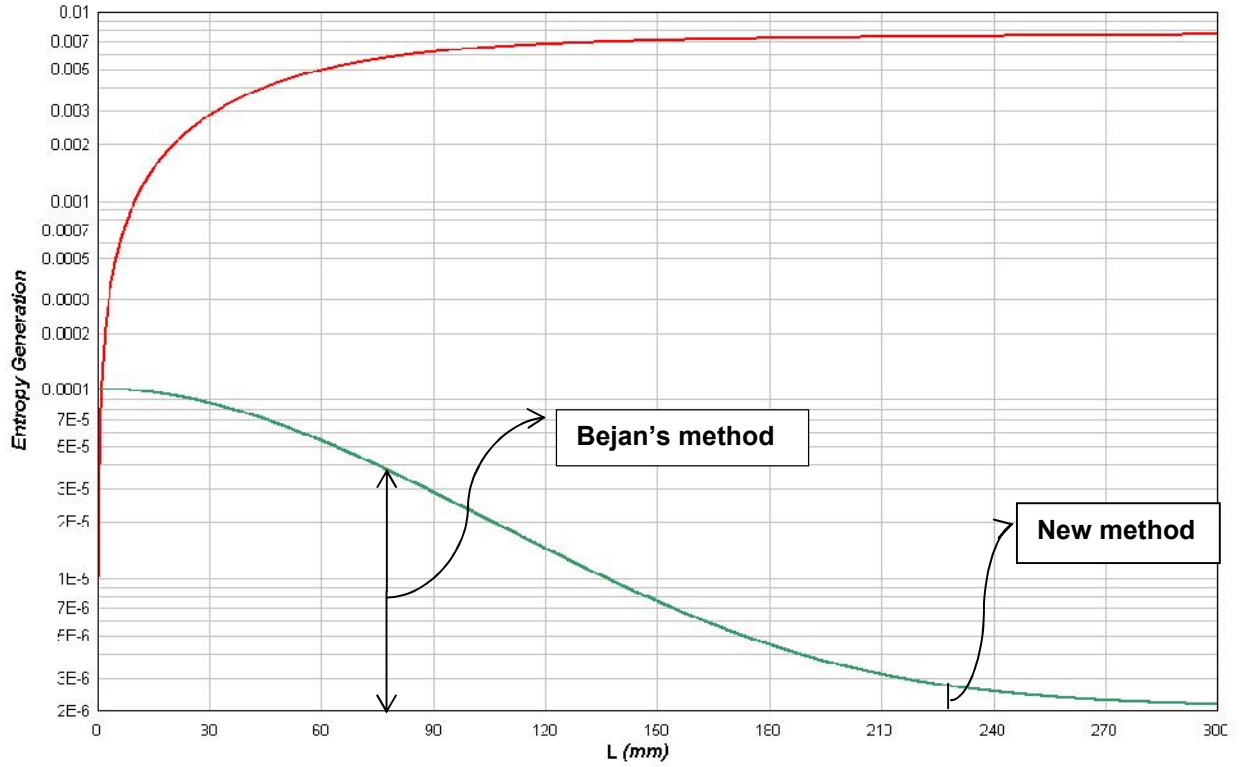


Fig.2. Function of entropy generation

In this figure the red graph is the function of the entropy generation, and the green one is the derivative of the entropy generation function. As it is evident from the Figure of (2) the entropy generation for the fin increases along the fin. However, from the $x=65$ mm onwards the entropy generation will be constant approximately, and based on the concept of entropy generation minimization the difference between the rate of the entropy generation at $x=63$ mm and 225 mm is negligible. The concept of entropy generation minimization dictates that when the function mentioned will be minimum that its derivative be zero. Referring to the green graph, it can be found that the difference to zero for the derivative of entropy generation function based on the Bejan model is very much compared with this new method. In addition, it is clear that when x is 63 mm the fin performance is not favorable, because the difference between fin and ambient temperature is so much, about 27°C . On the other hands, considering both temperature profile and entropy generation function simultaneously will reveal that when the fin temperature reaches to its optimum value, to have maximum rate of heat transfer, the entropy generation function will be constant ($x \geq 223$ mm). Furthermore, for a very long rod the rate of the entropy generation is:

$$\dot{S}_{gen} = \left\{ (hPkA_c)^{0.5} \cdot \left(\frac{T_b}{T_{\infty}} - 1 \right)^2 \right\} + \left\{ \frac{2.742(\rho D)^{0.754} \cdot U^{2.754} \cdot \mu^{0.246} \cdot L}{T_{\infty}} \right\} \quad (33)$$

$$D_{opt} = - \left\{ \frac{3.656\rho^{0.754} \cdot U^{2.754} \cdot \mu^{0.246} \cdot L \cdot T_{\infty}^2}{\theta_b^2 \sqrt{\pi^2 h k}} \right\}^{1.341} \quad (34)$$

Equation of (34) states that the length of the rod is so much as the rod diameter have to be negative value to the rate of the entropy generation be optimized, and this is another reason that the presented model has high accuracy in comparison to previous method.

5. CONCLUSION

Pin fins are widely used as effective elements for heat transfer enhancement. For this reason, extensive work has been carried out to select and optimize pin fins for various application such as electronic devices, chemical, food, and petrochemical industry. One of the strong tools in optimization, which has been introduced recently by Bejan, is entropy generation minimization. In this paper, some correlations to calculate the rate of entropy generation are offered for two boundary conditions, adiabatic and convection heat transfer. Then, the optimum fin length is presented for both boundary conditions. The accuracy of the model has been compared with experimental studies. The results showed high level of accuracy of the model, which can be used as a strong tool in optimization process of pin fins.

REFERENCES

1. Bejan, A.(1996) , Entropy Generation Minimization, CRC Press, New York.
2. Masoud Asadi and Dr R.H.Khoshkhoo, Investigation into radiation of a plate-fin heat exchanger with strip fins , Journal of Mechanical Engineering Research, April 2013, pp: 82-89.
3. Masoud Asadi and Dr R.H.Khoshkhoo, Entropy Generation in a Plate-Fin Compact Heat Exchanger with Louvered Fins , International Journal Energy Engineering, March 2013, pp: 110-118.
4. Masoud Asadi and Nasrin Dindar Mehrabani, Minimization entropy generation into compact heat exchanger with Louvered fins , Journal of Petroleum and Gas Engineering, 2013, pp: 35-45.
5. Masoud Asadi and Dr R.H.Khoshkhoo, Effects of mass flow rate in terms of pressure drop and heat transfer characteristics , Merit Research Journal of Environmental Science and Toxicology Vol. 1(1), February, 2013, pp: 5-11
6. N. Sahiti, F. Krasniqi, Xh. Fejzullahu, J. Bunjaku, A. Muriqi , Entropy generation minimization of a double-pipe pin fin heat exchanger , Applied Thermal Engineering, Volume 28, Issues 17–18, December 2008, Pages 2337-2344.
7. Paisarn Naphon , On the performance and entropy generation of the double-pass solar air heater with longitudinal fins , Renewable Energy, Volume 30, Issue 9, July 2005, Pages 1345-1357.
8. E. Ibrahim, M. Moawed , Forced convection and entropy generation from elliptic tubes with longitudinal fins , Energy Conversion and Management, Volume 50, Issue 8, August 2009, Pages 1946-1954.
9. Christian J.L. Hermes, Waldyr de Lima e Silva Jr., Felipe A.G. de Castro , Thermal-hydraulic design of fan-supplied tube-fin condensers for refrigeration cassettes aimed at minimum entropy generation , Applied Thermal Engineering, Volume 36, April 2012, Pages 307-313.
10. Lina Zhang, Chunxin Yang, Jianhui Zhou , A distributed parameter model and its application in optimizing the plate-fin heat exchanger based on the minimum entropy generation , International Journal of Thermal Sciences, Volume 49, Issue 8, August 2010, Pages 1427-1436.
11. İhsan Dağtekin, Hakan F. Öztıp, Ahmet Z. Şahin , An analysis of entropy generation through a circular duct with different shaped longitudinal fins for laminar flow , International Journal of Heat and Mass Transfer, Volume 48, Issue 1, January 2005, Pages 171-181.
12. Huee-Youl Ye, Kwan-Soo Lee , Refrigerant circuitry design of fin-and-tube condenser based on entropy generation minimization , International Journal of Refrigeration, Volume 35, Issue 5, August 2012, Pages 1430-1438.

13. Chin-Hsiang Cheng, Wen-Hsiung Huang , Entropy generation and heat transfers via laminar forced-convection channel flows over transverse fins in entrance regions , *Applied Energy*, Volume 32, Issue 4, 1989, Pages 241-267.
14. Chin-Hsiang Cheng, Wei-Ping Ma, Wen-Hsiung Huang , Numerical predictions of entropy generations for mixed convective flows in a vertical channel with transverse fin array , *International Communications in Heat and Mass Transfer*, Volume 21, Issue 4, July–August 1994, Pages 519-530.
15. Aggrey Mwesigye, Tunde Bello-Ochende, Josua P. Meyer , Numerical investigation of entropy generation in a parabolic trough receiver at different concentration ratios , *Energy*, Volume 53, 1 May 2013, Pages 114-127.
16. T.H. Ko, C.P. Wu , A numerical study on entropy generation induced by turbulent forced convection in curved rectangular ducts with various aspect ratios , *International Communications in Heat and Mass Transfer*, Volume 36, Issue 1, January 2009, Pages 25-31.
17. Zhou Jian-hui, Yang Chun-xin, Zhang Li-na , Minimizing the entropy generation rate of the plate-finned heat sinks using computational fluid dynamics and combined optimization , *Applied Thermal Engineering*, Volume 29, Issues 8–9, June 2009, Pages 1872-1879.
18. Xiao Wang, Jianlin Yu, Ming Ma , Optimization of heat sink configuration for thermoelectric cooling system based on entropy generation analysis , *International Journal of Heat and Mass Transfer*, Volume 63, August 2013, Pages 361-365.
19. T.H. Ko, K. Ting , Entropy generation and optimal analysis for laminar forced convection in curved rectangular ducts: A numerical study , *International Journal of Thermal Sciences*, Volume 45, Issue 2, February 2006, Pages 138-150.
20. Elisa Guelpa, Adriano Sciacovelli, Vittorio Verda , Entropy generation analysis for the design improvement of a latent heat storage system , *Energy*, Volume 53, 1 May 2013, Pages 128-138.
21. T.-H. Ko , A numerical study on entropy generation and optimization for laminar forced convection in a rectangular curved duct with longitudinal ribs , *International Journal of Thermal Sciences*, Volume 45, Issue 11, November 2006, Pages 1113-1125.
22. K. Hooman, H. Gurgenci, A.A. Merrikh , Heat transfer and entropy generation optimization of forced convection in porous-saturated ducts of rectangular cross-section , *International Journal of Heat and Mass Transfer*, Volume 50, Issues 11–12, June 2007, Pages 2051-2059.
23. Gamze Gediz Ilis, Moghtada Mobedi, Bengt Sundén , Effect of aspect ratio on entropy generation in a rectangular cavity with differentially heated vertical walls , *International Communications in Heat and Mass Transfer*, Volume 35, Issue 6, July 2008, Pages 696-703.
24. A.C. Baytaş , Entropy generation for natural convection in an inclined porous cavity , *International Journal of Heat and Mass Transfer*, Volume 43, Issue 12, 15 June 2000, Pages 2089-2099.
25. Nwachukwu P. Nwosu , Employing exergy-optimized pin fins in the design of an absorber in a solar air heater , *Energy*, Volume 35, Issue 2, February 2010, Pages 571-575.
26. Guillermo Ibáñez, Aracely López, Joel Pantoja, Joel Moreira, Juan A. Reyes , Optimum slip flow based on the minimization of entropy generation in parallel plate microchannels , *Energy*, Volume 50, 1 February 2013, Pages 143-149.
27. Aung Myat, Kyaw Thu, Young Deuk Kim, Bidyut Baran Saha, Kim Choon Ng , Entropy generation minimization: A practical approach for performance evaluation of temperature cascaded co-generation plants , *Energy*, Volume 46, Issue 1, October 2012, Pages 493-521.
28. Wen-Jei Yang, Takahiro Furukawa, Shuichi Torii, Optimal package design of stacks of convection-cooled printed circuit boards using entropy generation minimization method , *International Journal of Heat and Mass Transfer*, Volume 51, Issues 15–16, 15 July 2008, Pages 4038-4046.

29. K.Y. Leong, R. Saidur, T.M.I. Mahlia, Y.H. Yau , Entropy generation analysis of nanofluid flow in a circular tube subjected to constant wall temperature , *International Communications in Heat and Mass Transfer*, Volume 39, Issue 8, October 2012, Pages 1169-1175.
30. Eiyad Abu-Nada , Investigation of entropy generation over a backward facing step under bleeding conditions , *Energy Conversion and Management*, Volume 49, Issue 11, November 2008, Pages 3237-3242.
31. C. Balaji, M. Hölling, H. Herwig , Entropy generation minimization in turbulent mixed convection flows , *International Communications in Heat and Mass Transfer*, Volume 34, Issue 5, May 2007, Pages 544-552.
32. M. Bidi, M.R.H. Nobari, M. Saffar Avval , A numerical evaluation of combustion in porous media by EGM (Entropy Generation Minimization) , *Energy*, Volume 35, Issue 8, August 2010, Pages 3483-3500.
33. R.T. Ogulata, F. Doba , Experiments and entropy generation minimization analysis of a cross-flow heat exchanger , *International Journal of Heat and Mass Transfer*, Volume 41, Issue 2, January 1998, Pages 373-381.
34. T.H. Ko, C.S. Cheng , Numerical investigation on developing laminar forced convection and entropy generation in a wavy channel , *International Communications in Heat and Mass Transfer*, Volume 34, Issue 8, October 2007, Pages 924-933.
35. XueTao Cheng, XinGang Liang, Discussion on the applicability of entropy generation minimization to the analyses and optimizations of thermodynamic processes , *Energy Conversion and Management*, Volume 73, September 2013, Pages 121-127.
36. Jiangfeng Guo, Lin Cheng, Mingtian Xu , Optimization design of shell-and-tube heat exchanger by entropy generation minimization and genetic algorithm , *Applied Thermal Engineering*, Volume 29, Issues 14–15, October 2009, Pages 2954-2960.
37. Enrico Sciubba , A minimum entropy generation procedure for the discrete pseudo-optimization of finned-tube heat exchangers , *Revue Générale de Thermique*, Volume 35, Issue 416, September 1996, Pages 517-525.
38. Assunta Andreozzi, Antonio Auletta, Oronzio Manca , Entropy generation in natural convection in a symmetrically and uniformly heated vertical channel , *International Journal of Heat and Mass Transfer*, Volume 49, Issues 17–18, August 2006, Pages 3221-3228.
39. McClintock.F.A, The design of heat exchangers for minimum irreversibilities, ASME paper NO.51-A-108.1952.
40. Poulikakos.D and Bejan.A, Fin geometry for minimum entropy generation in forced convection, *Journal of Heat Transfer*, Vol 104, 1982, pp: 616-623.
41. Lee, J. H., Kwon, Y. C., and Kim, M. H., An Improved Method for Analyzing a Fin and Tube Evaporator Containing a Zeotropic Mixture Refrigerant with Air Maldistribution, *International Journal of Refrigeration*, vol. 26, no. 6, pp. 707–720, 2003.
42. H. Jiang, R. Radermacher, and V. Aute, A User-Friendly Simulation And Optimization Tool For Design Of Coils, *International Refrigeration and Air Conditioning Conference.2002*, Paper 546.
43. N. Sahiti, F. Krasniqi, Xh. Fejzullahu, J. Bunjaku, A. Muriqi, Entropy generation minimization of a double-pipe pin fin heat exchanger, *Applied Thermal Engineering*, Volume 28, Issues 17–18, December 2008, Pages 2337-2344.
44. Christian J.L. Hermes, Waldyr de Lima e Silva Jr., Felipe A.G. de Castro, Thermal-hydraulic design of fan-supplied tube-fin condensers for refrigeration cassettes aimed at minimum entropy generation, *Applied Thermal Engineering*, Volume 36, April 2012, Pages 307-313.
45. E. Ibrahim, M. Moawed, Forced convection and entropy generation from elliptic tubes with longitudinal fins, *Energy Conversion and Management*, Volume 50, Issue 8, August 2009, Pages 1946-1954.
46. Lina Zhang, Chunxin Yang, Jianhui Zhou, A distributed parameter model and its application in optimizing the plate-fin heat exchanger based on the minimum entropy

generation, *International Journal of Thermal Sciences*, Volume 49, Issue 8, August 2010, Pages 1427-1436.

47. Huee-Youl Ye, Kwan-Soo Lee, Refrigerant circuitry design of fin-and-tube condenser based on entropy generation minimization, *International Journal of Refrigeration*, Volume 35, Issue 5, August 2012, Pages 1430-1438.

48. Giorgio Giangaspero, Enrico Sciubba, Application of the entropy generation minimization method to a solar heat exchanger: A pseudo-optimization design process based on the analysis of the local entropy generation maps, Available online 4 March 2013.

49. Bruno F. Pussoli, Jader R. Barbosa Jr., Luciana W. da Silva, Massoud Kaviany, Optimization of peripheral finned-tube evaporators using entropy generation minimization, *International Journal of Heat and Mass Transfer*, Volume 55, Issues 25–26, December 2012, Pages 7838-7846.

50. Zhou Jian-hui, Yang Chun-xin, Zhang Li-na, Minimizing the entropy generation rate of the plate-finned heat sinks using computational fluid dynamics and combined optimization, *Applied Thermal Engineering*, Volume 29, Issues 8–9, June 2009, Pages 1872-1879.

51. Gamze Gediz Ilis, Moghtada Mobedi, Bengt Sunden, Effect of aspect ratio on entropy generation in a rectangular cavity with differentially heated vertical walls, *International Communications in Heat and Mass Transfer*, Volume 35, Issue 6, July 2008, Pages 696-703.

52. Aggrey Mwesigye, Tunde Bello-Ochende, Josua P. Meyer, Numerical investigation of entropy generation in a parabolic trough receiver at different concentration ratios, *Energy*, Volume 53, 1 May 2013, Pages 114-127.

53. Wenhua Li, Shenglan Xuan, Jian Sun, Entropy generation analysis of fan-supplied gas cooler within the framework of two-stage CO₂ transcritical refrigeration cycle, *Energy Conversion and Management*, Volume 62, October 2012, Pages 93-101.