1 2	Original Research Artic Effects of Suction and Thermal Radiation on Heat transfer in a Third Grade Fluid over		
3	Vertical Plate		
4	Abstract		

5 An analysis is presented to investigate the effects suction and thermal radiation on the unsteady 6 convective flow and heat transfer in a third grade fluid over an infinite vertical plate. The plate is 7 porous to allow for possible wall suction. The governing time-based coupled partial differential equations, subjected to their boundary conditions, are solved numerically by applying an 8 9 efficient and unconditionally stable Crank-Nicolson finite difference scheme. Numerical calculations are carried out for different values of dimensionless parameters in the problem. An 10 analysis of the results obtained reveals that the flow field is appreciably influenced by suction 11 12 and viscoelastic parameters. An increase in the suction parameter is observed to decrease the fluid velocity. It also shows that the temperature distribution decreases with an increase in the 13 thermal radiation parameter. 14

15 Keywords - Suction, Thermal Radiation, Heat Transfer, Porous Plate, Third Grade Fluid.

16 1. INTRODUCTION

Non-Newtonian fluids have been a subject of great interest to researchers because of their various industrial and enginnering applications. Unlike the viscous fluids, the non-Newtonian fluids cannot be described by the single constitutive relationship between the stress and the strain rate. This is due to diverse features of such fluids in nature. Generally, the mathematical problems in non-Newtonian fluids are more complicated because of its nonlinear and higher-

order than those in Newtonian fluids. Despite these complexities of non-Newtonian fluids,scientists and engineers are engaged in non-Newtonian fluid dynamics.

Erdogan (1995) analyzed the flow of a third grade fluid in the vicinity of a plane wall suddenly 24 set in motion. He observed that for a short time, a strong non-Newtonian effect was present in 25 26 the velocity field. However, for a long time, the velocity field became Newtonian. The problem of peristaltic flow of MHD third order fluid in a planar channel with slip condition was 27 investigated Hayat et al. (2011). The pumping and trapping phenomena are analyzed in the 28 presence of MHD and slip effects. They derived the solutions under long wavelength and low 29 30 Reynold's number approximations. Hayat et al. (2006) also gave the solution for the flow of a 31 third grade fluid bounded by two parallel porous plates using homotopy analysis method. They 32 made a comparison with the exact numerical solution for the various values of the physical parameters. 33

34 Sajid and Hayat (2007) also presented solution to two-dimensional boundary layer flow of the third grade fluid over a stretching sheet. Sajid et al. (2007) further considered heat transfer 35 characteristics in an electrically conducting third grade fluid. Non-similar analytic solution for 36 37 MHD flow and heat transfer in a third order fluid over a stretching sheet was considered by Sajid et al. (2007). Siddiqui et al. (2008) presented the heat transfer flow problem of a third grade fluid 38 between two heated parallel plates for the constant viscosity model. Three flow problems of 39 Couette flow, plane Poiseuille flow and plane Couette-Poiseuille flow were considered by them 40 and they employed the homotopy perturbation technique to obtain their results. Hayat et al. 41 (2008) presented exact solutions of the thin film flow problem for a third grade fluid on an 42 inclined plane. They compared their results with those of Siddiqui et al. (2006) and concluded 43 that their solutions were valid for large values of the material parameter. 44

45 Also, one can refer to some useful works of Hayat and his co-workers in [10-16], regarding the flow and heat transfer in a third grade fluid with different geometries and diverse physical 46 characteristics. Sahoo (2009) numerically studied the problem of Heimenz flow and heat transfer 47 of a third grade fluid using the finite difference technique with Richardson is extrapolation. 48 Ellahi et al. (2010) examined the heat transfer analysis on the laminar flow of an incompressible 49 third grade fluid through a porous flat channel. They provided analytical solution for temperature 50 distribution for various values of the controlling parameters, compared the results obtained with 51 the numerical solution and the comparison showed the fact that the accuracy is remarkable. The 52 series solution to the unsteady boundary layer flow of the third grade fluid was developed by 53 Abbasbandy and Hayat (2011). 54

Ellahi and Hamed (2012) numerically investigated the steady non-Newtonian flows with heat 55 transfer, MHD and nonslip effects. Navat et al. (2012) studied the flow and heat transfer of a 56 57 third grade fluid past a porous vertical plate. They obtained solutions through numerical approach. Sibanda et al. (2012) studied the problem of heat transfer flow of a third grade fluid 58 between parallel plates using the spectral homotopy analysis method. Explicit analytical 59 60 expressions for the non-linear momentum reaction the energy equation were solved using the homotopy perturbation method. Recently, Hayat et al. (2013) carried out an analysis for the 61 characteristics of melting heat transfer in the boundary layer flow of third grade fluid in a region 62 of stagnation point past a stretching sheet. They developed the series solutions by homotopy 63 analysis method and compared their results with the previous studies. Baoku et al. (2013) 64 reported the solution to the problem of MHD partial slip flow, heat and mass transfer of a 65 viscoelastic third grade fluid over an insulated porous plate embedded in a porous medium. They 66 presented numerical experiments to solve the governing coupled highly nonlinear ordinary 67

differential equations of momentum, energy and concentration showing the effects of the variousphysical parameters on the velocity, temperature and concentration distributions.

The influence of thermal radiation on flow and heat transfer processes is paramount in the design 70 of many advanced energy conversion systems operating at high temperature. [Seddeek (2002)]. 71 Thermal radiation within such systems occurs because of the emission by the hot walls and 72 working fluid. Plumb et al. (1981) studied the effect of horizontal cross-flow and radiation on 73 natural convection from vertical heat surface in saturated porous media. Rosseland diffusion 74 approximation was utilized for the convective flow with radiation. Hossain and Takhar (1996), 75 Takhar et al. (1996), Hossain et al. (1999) extensively investigated the effect of radiation on heat 76 transfer problems. Mansour (1997) analyzed combined forced-convective flow over a flat plate 77 immersed in porous medium of variable viscosity. Sajid and Hayat (2008) examined the problem 78 79 of radiation effects on the flow over an exponentially stretching sheet and solved the problem analytically using the homotopy analysis method. The numerical solution for the problem was 80 then provided Bidin and Nazar (2009). Anand Rao et al. (2012) studied radiation effects on an 81 unsteady MHD free convective flow past a vertical porous plate in the presence of soret effect. 82 Seethamahalakshmi et al. (2011) investigated the unsteady MHD free convective flow and mass 83 transfer near a moving vertical plate in the presence of thermal radiation. Other research works 84 that have been carried out on this are those of Makinde et al. (2011), Srinivas and Muthuraj 85 (2010) and Singh et al. (2010). Baoku et al. (2012) recently investigated the influence of thermal 86 radiation on a transient magnetohydrodynamic Couette flow of a high Prandtl number fluid with 87 temperature-dependent viscosity through a porous medium. They employed an implicit finite 88 difference scheme of Crank-Nicolson type to investigate the effects of pertinent flow parameters. 89

The aim of this study is to investigate the suction and thermal radiation effects in a 90 thermodynamically compatible viscoelastic third grade fluid on unsteady flow and convective 91 heat transfer over an infinite plate which is set in motion with an oscillating temperature applied 92 93 to the plate. The governing coupled nonlinear partial differential equations with sufficient initial and boundary conditions are solved by employing Crank-Nicolson finite different scheme with 94 modified Newton's method. The present problem with radiative heat flux has not been 95 considered in the scientific literature, despite its important applications in industry and 96 engineering. 97

98 2. Mathematical Analysis

We consider the transient flow and heat transfer of an incompressible fluid of a third grade past infinite porous plate. The x'- axis is taken along the plate vertically upwards and y'- axis is normal to it. The plate is suddenly set in motion in its own plane with a velocity U(t). An oscillating temperature is assumed to be applied on the plate in the presence of thermal radiation. We assume the plate is infinitely long, the physical variables are functions of y' and t' only. Hence, from the continuity equation, the velocity field is described as:

105

$$u' = u'(y', t'), v' = -V_0$$
 (1)

106 where u' and v' are the velocities of the fluid along x' and y' axes respectively and $V_0 > 0$ 107 indicates suction velocity.

108

110 **2.1 Flow Analysis**

The constitutive equation of an incompressible third grade fluid as given by Coleman and Noll 111 (1965) is: 112

113
$$\tau' = -pI + \sum_{i=1}^{3} S_i$$
 (2)

where $S_1 = \mu A_1$, $S_2 = \alpha_1 A_2 + \alpha_2 A_1^2$ and $S_3 = \beta_1 A_3 + \beta_2 (A_2 A_1 + A_1 A_2) + \beta_3 (trA_2)A_1$. 114

 $\mu, \alpha_1, \alpha_2, \beta_1, \beta_2, \beta_3$ being material constants, τ' the stress-tensor, p the pressure, I the identity 115

tensor and A_n represents the kinematical tensors defined by, $A_0 = I$, $A_1 = \nabla u + (\nabla u)^T$, 116

117
$$A_{n+1} = \left(\frac{\partial}{\partial t} + u \cdot \nabla\right) A_n + \nabla u \cdot A_n + \left(\nabla u \cdot A_n\right)^T, \ n = 1, 2.$$

where u is the velocity and t is the time. A detailed thermodynamic analysis of the model, 118 represented by (2) is given by Fosdick and Rajagopal (1980). It was shown that if all the motions 119 120 of the fluid are to be compatible with thermodynamics in the sense that these motions meet the 121 Clausius-Duhem inequality and if it is assumed that the specific Helmholtz free energy is a 122 minimum when the fluid is locally at rest, then

,

123
$$\mu \ge 0, \ \alpha_1 \ge 0, \ |\alpha_1 + \alpha_2| \le \sqrt{24\mu\beta_3}, \ \beta_1 = \beta_2 = 0, \ \beta_3 \ge 0 \text{ and}$$

124
$$\tau' = -pI + \mu_1 A_1 + \alpha_1 A_2 + \alpha_2 A_1^2 + \beta_3 (tr A_1^2) A_1$$
(2^{*})

The stress components (2^*) by virtue of equation (1) are: 125

126
$$\tau_{x'x'} = -p + \alpha_2 \left(\frac{\partial u'}{\partial y'}\right)^2 + 2\beta_2 \frac{\partial u'}{\partial y'} \frac{\partial^2 u'}{\partial y' \partial t'},$$
127
$$\tau_{y'y'} = -p + \left(2\alpha_1 + \alpha_2\right) \left(\frac{\partial u'}{\partial y'}\right)^2 + \left(6\beta_1 + 2\beta_2\right) \frac{\partial u'}{\partial y'} \frac{\partial^2 u'}{\partial y' \partial t'},$$
128
$$\tau_{z'z'} = -p,$$
(3)

129
$$\tau_{x'y'} = \mu \frac{\partial u'}{\partial y'} - \alpha_1 V_0 \frac{\partial^2 u'}{\partial y'^2} + \alpha_1 \frac{\partial^2 u'}{\partial y' \partial t'} + 2(\beta_2 + \beta_3) \left(\frac{\partial u'}{\partial y'}\right)^3 + \beta_1 \left(\frac{\partial^3 u'}{\partial y' \partial t'^2}\right)$$

130
$$au_{x'z'} = au_{z'y'} = 0$$

131 where
$$\tau_{x'y'} = \tau_{y'x'}$$
, $\tau_{x'z'} = \tau_{z'x'}$, $\tau_{y'z'} = \tau_{z'y'}$

132 Inserting the stress components and velocity given by (1) in the equation of motion:

133
$$\rho \frac{Dv_i}{Dt} = -\tau_{,i} + \rho X_i + \tau_{ij,j}$$
 (4)

where $\frac{D}{Dt}$ denotes the material derivative and X_i is the external force per unit mass in i^{th} direction, the governing equation of free convective flow field under the physical conditions of the problem is obtained as:

137
$$\rho\left(\frac{\partial u'}{\partial t'} - V_0 \frac{\partial u'}{\partial y'}\right) = \mu \frac{\partial^2 u'}{\partial y'^2} + \alpha_1 \left(\frac{\partial^3 u'}{\partial y'^2 \partial t'} - V_0 \frac{\partial^3 u'}{\partial y'^3}\right) + 6\beta_3 \left(\frac{\partial u'}{\partial y'}\right)^2 \frac{\partial^2 u'}{\partial y'^2} + \rho \beta_T g \left(T' - T'_{\infty}\right)$$
(5)

139 2.2 Heat Transfer Analysis

140 Neglecting viscous dissipation, the heat transport equation is obtained as:

141
$$\rho C_p \frac{DT}{Dt} = K \nabla^2 T - \nabla q_r$$
(6)

142 Assuming the conditions of optically thin environment that the radiative heat flux, $\frac{\partial q'}{\partial y'}$ in the

143 energy equation takes the form Takhar, et al.(1996):
$$\frac{\partial q'}{\partial y'} = 4\eta^2 (T' - T'_{\infty})$$
 where $\eta^2 = \int_0^\infty \left(\delta\lambda \frac{\partial B}{\partial T'}\right)$;

144 η^2 , δ , λ and *B* are respectively absorption coefficient, radiation absorption coefficient, 145 frequency and Planck's constant, the governing equation of temperature flow field is obtained as:

146
$$\rho C_{p} \left(\frac{\partial T'}{\partial t'} - V_{0} \frac{\partial T'}{\partial y'} \right) = K \frac{\partial^{2} T'}{\partial y'^{2}} - 4\eta^{2} \left(T' - T_{\infty}' \right)$$
(7)

In the energy equation (6), the term representing viscous and joule dissipation are assumed to beneglected as they are really very small in slow motion free convection flows.

149 The initial and boundary conditions are:

150
$$t' \le 0: y = 0, u' = 0, T' = 0,$$

151
$$t' \succ 0: u' = U(t') = \frac{U^{2n+1}}{v^n} \ell^{a't'} t'^n$$
, when $y' = 0$

152
$$T' = T'_{\infty} + (T'_{w} - T'_{\infty})\cos\omega' t', when y' = 0$$
 (8)

153
$$u' = 0$$
, when $y \to \infty$, $\frac{\partial u'}{\partial y'} = 0$, when $y \to \infty$

154
$$T' = T'_{\infty}$$
, when $y' \to 0$

155 For computing the solution, we choose $U(t') = \frac{U^{2n+1}}{v^n} \ell^{a't'} t'^n$ where $v = \frac{\mu}{\rho}$ is the kinematic

156 coefficient of viscosity. We introduce the following dimensionless variables:

157
$$u = \frac{u'}{U}$$
, $y = \frac{y'U}{v}$, $a = \frac{a'v}{U^2}$, $t = \frac{t'U^2}{v}$, $b = \frac{b'v}{U^2}$, $\omega = \frac{V_0}{U}$,

158
$$\alpha = \frac{\alpha_1 U^2}{\rho v^2}, \quad \beta = \frac{6\beta_3 U^4}{\rho v^3}, \quad \Pr = \frac{v\rho C_p}{K}, \quad \theta = \frac{T' - T'_{\infty}}{T'_w - T'_{\infty}}, \quad Gr = \frac{\beta_g v (T'_w - T'_{\infty})}{U^3}, \quad R_d = \frac{4\eta^2 v}{\rho C_p U^2}$$

159 Using the above equation parameters, equations (5) and (7) reduce to:

160
$$\frac{\partial u}{\partial t} - \omega \frac{\partial u}{\partial y} = \frac{\partial^2 u}{\partial y^2} + \alpha \frac{\partial^3 u}{\partial y^2 \partial t} - \omega \alpha \frac{\partial^3 u'}{\partial {y'}^3} + \beta \left(\frac{\partial u}{\partial y}\right)^2 \frac{\partial^2 u}{\partial y^2} + Gr\theta$$
(9)

161
$$\frac{\partial \theta}{\partial t} = \omega \frac{\partial \theta}{\partial y'} + \frac{1}{\Pr} \frac{\partial^2 \theta}{\partial y^2} - R_d \theta$$
(10)

162 The initial and boundary conditions now become:

163 $t \le 0: y = 0, u = 0, \theta = 0;$

164
$$t \succ 0: u = U(t) = \ell^{at} t^n$$
, when $y = 0$;

165
$$\theta = \cos bt$$
, when $y = 0$; (11)

166
$$u = 0, when y \to \infty, \frac{\partial u}{\partial y} = 0, when y \to \infty; \theta = 0, when y \to \infty;$$

167 **3.** Numerical Procedure

The governing nonlinear coupled partial differential equations (9) and (10) with the initial and boundary conditions (11) are solved by employing Crank-Nicolson finite difference scheme which has been discussed by Ganesan and Palani (2002), Conte and De Boor (1980), Jain (1984) and Baoku, et al. (2012). We therfore discretized the governing equations based on the unsteady state conditions. The numerical method of Crank-Nicolson type does not restrict the value of rto be chosen. The finite difference equations corresponding to these equations are given as:

174
$$u_{i,j+1} - u_{i,j} = \left(\frac{\omega r h}{4} + \frac{r}{2} + \frac{\alpha}{h^2} - \frac{\omega \alpha r}{h}\right) u_{i+1,j+1} + \left(\frac{r}{2} - \frac{\omega r h}{4} + \frac{\alpha}{h^2} - \frac{\omega \alpha r}{h}\right) u_{i-1,j+1}$$

175
$$+\left(\frac{\omega r h}{4}+\frac{r}{2}\right)u_{i+1,j}+\left(\frac{r}{2}-\frac{\omega r h}{4}+\frac{\alpha}{h^2}\right)u_{i-1,j}-2\left(\frac{r}{2}+\frac{\alpha}{h^2}\right)u_{i,j+1}-2\left(\frac{r}{2}+\frac{\alpha}{h^2}\right)u_{i,j}$$

176
$$+ \frac{\alpha}{h^2} u_{i+1,j} - \frac{\omega \alpha r}{2h} \left(-u_{i-2,j+1} + u_{i+2,j+1} + u_{i-2,j} - 2u_{i-1,j} + 2u_{i+1,j} - u_{i+2,j} \right)$$
(13)

177
$$+ \frac{\beta r}{32h} \begin{bmatrix} (u_{i+1,j+1})^2 + (u_{i-1,j+1})^2 + (u_{i+1,j})^2 + (u_{i-1,j})^2 - 2u_{i+1,j+1}u_{i-1,j-1} + 2u_{i+1,j+1}u_{i+1,j} \end{bmatrix}$$

178
$$\left(u_{i+1,j+1} - 2u_{i,j+1} + u_{i-1,j+1} + u_{i+1,j} - 2u_{i,j} + u_{i-1,j}\right) + r \, Gr \, h^2 \theta_{i,j}$$

$$\mathbf{179} \qquad \boldsymbol{\theta}_{i,j+1} = \left(\frac{\omega r h}{2} + \frac{r}{\Pr}\right) \boldsymbol{\theta}_{i+1,j+1} + \left(\frac{r}{\Pr} - \frac{\omega r h}{2}\right) \boldsymbol{\theta}_{i-1,j+1} - \left(\frac{2r}{\Pr} + \frac{R_d r h^2}{2}\right) \boldsymbol{\theta}_{i,j+1} + \left(1 - \frac{R_d r h^2}{2}\right) \boldsymbol{\theta}_{i,j} \quad (14)$$

180 where *i* dessignates the grip point along *y*-direction, *j* along *t*-direction and $r = \frac{\Delta t}{h^2}$. Hence, 181 the equations of motion and energy are reduced to system of algebraic nonlinear coupled-

equations. The mesh size h is 0.05 with time step t = 0.1. The values of u(y,t) and $\theta(y,t)$ are known at all grip points when t = 0 from the initial conditions. Modified Newton's iterative technique is used to solve the system of nonlinear algebraic equations. Computations are carried out by moving along y-direction. After computing values corresponding to each i at a time level, the values at the next time level are determined in similar manner.

The implicit nature of Crank-Nicolson method is unconditionally stable and has local truncation 187 error $O((\Delta t)^2, h^2)$ which tends to zero as Δt and h^2 tend to zero. There is no drawback of 188 conditionally stability from one level to the next. The implicit method gives stable solutions and 189 requires iterative procedure which we did at step forward in time because this problem is an 190 initial-boundary value problem with a finite number of spatial grip points. Though, the 191 corresponding difference equations do not automatically guarantee the convergence of the mesh 192 $h \rightarrow 0$. To achieve maximum numerical efficiency, we used the tridiagonal procedure to solve 193 the two point conditions for (10) and four point conditions for (9). We tansformed the above 194 procedure into Maple code as described by Heck (2003), the convergence of the process was 195 quite satisfactory and the numerical stability of the method was guaranteed by the implicit nature 196 of the scheme. Hence, the scheme is consistent; stability and consistency ensure convergence. 197

198 4. Discussion of Results

The investigation focuses on the flow fields when a vertically upward plate suddenly starts moving with a velocity in its own plane and temperature fields assumed to be oscillating applied to the plate in the presence of suction and thermal radiation. The governing equations of the flow and temperature fields are solved using Crank-Nicolson implicit finite difference scheme with modified Newton's method and approximate solutions are obtained for the velocity and
tempearture profiles. The effects of the pertinent parameters on the flow and temperature fields
are analyzed and discussed with the help of velocity profiles (Figures 1 - 5) and temperature
profiles (Figures 6 - 8).

207 4.1 Velocity Profiles

The effects of various parameters on the velocity field are investigated through simulations using 208 the method above and results are produced as graphs for two major cases; n = 0.8, i.e. when the 209 210 plate starts moving with variable acceleration and n=1, i.e. when the plate starts with a constant acceleration. Figure 1 analyzes the influence of suction parameter ω for cases n = 0.8211 212 and n = 1. It is observed that an increase in the suction parameter ω decreases the fluid velocity at any point of the fluid, and higher velocity profile is attained when n = 0.8. Figures 2 and 3 213 depict the effect of viscoelastic parameters α and β on the velocity field. It is observed that as a 214 growing viscoelastic parameter α increases, the velocity field increases. The influence of β on 215 the velocity profile is noticeable when there is small increment in time interval. An increase in 216 β corresponds to a growing in the velocity profiles for both cases of constant and variable 217 accelerations. As the free convection current exists by virtue of temperature difference $(T' - T'_{\infty})$, 218 the Grashof number Gr can realistically take any real number when $0 \le b \le \frac{\pi}{2}$. Gr > 0 219

corresponds to cooling of the plate and $Gr \prec 0$ corresponds to heating of the plate due to free convection current. Therefore, we have chosen both positive and negative values of Grashof number. An increase in Grashof number Gr increases the fluid velocity near the plate when the plate is being heated for both n = 0.8 and n = 1 in Figure 4. However, when the plate is being cooled, the fluid velocity decreases as the Grashof number increases. Also, Figures 5 shows that
an increase in Prandtl number Pr increases the fluid velocity in both cases of constant and
variable accelerations.

Figures 1-5 should be here.

228 4.2 Temperature Fields

229 The temperature of the flow field suffers a substantial change with the variation of the flow parameters such as suction parameter ω , Prandtl number Pr and thermal radiation 230 parameter R_d . These variations are shown in Figures 6 – 8. Figure 6 depicts the influence of 231 suction parameter ω on the temperature profile. A growing ω is found to decrease the 232 temperature of the flow field at all points in the domain. Similarly, it is observed in Figure 7 that 233 234 the effect of increasing Pr reduces the temperature field. Lastly, it is evident from Figure 8 that at lower value of R_d , there little or no influence of R_d on the temperature profile whereas at 235 236 higher value of R_d , the effect of R_d on temperature distribution is noticeable. Hence, the consequence of increasing R_d has the influence of decreasing the temperature of the flow field. 237

238 Figures 6-8

239 **5.** Conclusions

In this study, we investigate the influence of suction and thermal radiation on the transient flow and heat transfer of a third grade viscoelastic fluid through a vertical porous plate employing an implicit finite difference numerical scheme of Crank-Nicolson type to discretize the system of coupled partial diffential equations and modified Newton's method to solve the system of

algebraic nonlinear equations obtained after discretization. The above scheme is transformed into
the Maple code to simulate the solutions of the problem. This solution procedure is valid for all
values of viscoelastic parameters unlike perturbation and power series methods that are only
valid for small values of viscoelastic parameters.

We therefore summarize below the following results of physical interest on the velocity and temperature distribution of the flow field:

- 250 The fluid velocity increases when the value of the second grade viscoelastic parameter α 251 increases. Also, it increases with an increase in the third grade viscoelastic parameter β 252 for small increment in the time interval.
- 253 \succ The suction parameter ω has the influence of reducing the velocity and temperature 254 field.
- As the Prandtl number increases, it also increases the velocity field but it reduces the temperature distribution of the flow field.
- 257 > The fluid velocity increases when the plate is being heated and decreases when the plate
 258 is being cooled with higher velocity profile noticeable when the plate starts moving with
 259 variable acceleration.
- 260 > The effect of increasing the thermal radiation parameter R_d decreases the temperature 261 distribution of the flow field.
- 262

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Figure 1: Effect of ω on velocity field when n = 0.8 and n = 1 with $\alpha = 1$, $\beta = 1$, Gr = 10, Pr = 10.



Figure 2: Effect of α on velocity field when n = 0.8 and n = 1 with $\omega = 5$, $\beta = 1$, Gr = 10, Pr = 10.



389 Figure 3: Effect of β on velocity field when n = 0.8 and n = 1 with 390 $\alpha = 1, \omega = 5, Gr = 10, Pr = 10.$



Figure 4: Effect of *Gr* on velocity field when n = 0.8 and n = 1 with $\alpha = 1$, $\beta = 1$, $\omega = 10$, Pr = 10.



Figure 5: Effect of Pr on velocity field when n = 0.8 and n = 1 with $\alpha = 1$, $\beta = 1$, Gr = 10, $\omega = 5$.

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400 Figure 7: Effect of Pr on temperature field when $R_d = 5$ and $\omega = 5$.



